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Long Term Degradation of Polymide Composites

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LONG TERM DEGRADATION OF POLYMIDE COMPOSITES

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ABSTRACT

The durability of polymer matrix composites exposed to harsh environments is a major concern. Surface degradation and damage are observed in polyimide composites used in air at 125-300°C. It is believed that diffusion of oxygen into the material and oxidative chemical reactions are responsible. Previous work has characterized and modeled diffusion behavior, and thermogravimetric analyses (TGAs) have been carried out in nitrogen, air, and oxygen to provide quantitative information on thermal and oxidative reactions. However, the model developed using these data did not successfully extrapolate TGA data down to conditions seen in service. A test program that focuses on lower temperatures and makes use of isothermal tests was undertaken to achieve a better understanding of the degradation reactions under use conditions. A new, low-cost technique was developed to collect chemical degradation data for isothermal tests lasting over 200 hours in the temperature range 125-300°C. Results indicate complex behavior not captured by the previous model, including the presence of weight-adding reactions. Weight gain reactions dominated in the 125-225°C temperature range, while weight loss reactions dominated beyond 225°C. The data obtained from isothermal tests and earlier TGAs is used to develop an advanced model of the material behavior.

INTRODUCTION

Composite materials are widely used in applications where they are exposed to high temperatures, thermal cycling and air. The durability of composites under such exposure is not well understood. The design of composites for such applications can be significantly improved by modeling the various degradation phenomena in such materials [1]. This can be achieved through the development of a model which can incorporate known quantities such as laminate geometry, material properties, temperatures and chemical environment, and from these determine the material degradation state as a function of exposure time and position within the material [2]. A schematic of the desired coupled analysis which could provide this capacity is shown in Figure 1. Each module shown in the figure needs to be well understood in order to be able to predict composite behavior under environmental and thermal exposure. Efforts of several researchers have improved the understanding of these modules. In this research, we have focused on chemical degradation.

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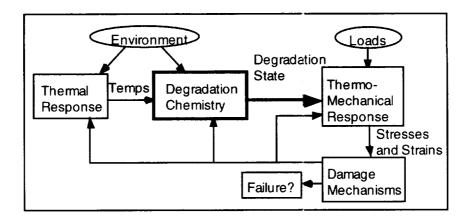


Figure 1. Comprehensive modeling flowchart

PREVIOUS WORK

It has been observed that macroscopic resin and composite specimens exposed to air at high temperatures develop a noticeable surface layer, and eventually damage such as crazing [3,4]. This is thought to be due to the combined effects of diffusion of oxygen into the material and chemical reaction [3]. This complicated multi-mechanism behavior makes interpretation of tests using macroscopic specimens difficult. Cunningham [1] separated diffusion and reaction effects by using finely ground powder specimens. This eliminates diffusion as a consideration, and allows work to be concentrated on the chemistry of degradation. Chemical degradation is also the focus of this work.

Work done by Cunningham [1] is reviewed here. TGA tests were carried out in nitrogen, air and oxygen for various heating rates. Powdered PMR-15 samples were heated from room temperature to 800°C. Mass loss and mass loss rate data was obtained from these experiments. An Arrhenius reaction based model was used for explaining this data. Two thermal and one oxidative reaction were used. The reaction coefficients were obtained from the data using Kissinger's method. The model worked well for high heating rates, but did not capture the behavior at lower heating rates. This model was also not able to explain the results of isothermal tests carried out in nitrogen, especially at lower temperatures (<300°C).

PROBLEM

The focus of this research is to develop a model of the chemical degradation of a polyimide matrix material composite such that, given the histories of chemical environment and temperature, we can calculate quantitative metrics of chemical degradation, as functions of time.

APPROACH

The approach consists of experimental and analytical work. Experiments were conducted with the aim of improving the understanding of the chemical degradation under service conditions and building an advanced model. As previous models had failed to explain the behavior during long term isothermal exposure, long term isothermal tests were conducted at various temperatures, in air, using a newly designed, low cost test apparatus. The experimental data was then used to obtain the coefficients of an advanced chemical model.

EXPERIMENTAL PROCEDURE

Powdered specimens were obtained from plaques of neat PMR-15 resin. A small amount of this fine powder was placed in a thermocycling oven and aged for a duration of about 200 hours. The sample was placed in an aluminum pan and weighed periodically to measure the mass loss (or gain) due to the chemical degradation. One specimen was tested at each of the temperatures. Specimens were aged in air.

MATERIAL PREPARATION

All material was manufactured at the NASA Lewis Research Center using standard manufacturing procedures developed for the PMR polyimides. The details of these procedures may be found in [5]. After curing, all specimens were subjected to a 16 hour free-standing post-cure in air at 316°C. Two PMR-15 neat resin plaques (both 102 mm x 102 mm (4" x 4") were used during this study. Specimens were taken from the neat resin plaques for use in the isothermal heating tests. Small strips were cut from the resin plaques and then powdered in a coffee grinder. A fine, light-brown powder was obtained. The powder was then sifted through a No. 40 sieve.

Tests conducted by Cunningham [1] had indicated that the particles obtained through the use of a No. 40 USA Standard Testing Sieve (425 micron grating) were sufficiently small to ensure that the effects of diffusion on the weight loss behavior in oxidative environments would be negligible. All powder produced in this manner was placed in small, unsealed glass jars and heated for 2 hours at 125°C to remove any residual moisture. The glass jars were immediately sealed after removal from the oven and the powder was stored like this until testing.

PROCEDURE

All powdered neat resin samples were aged in a thermal chamber. The chamber used electric resistance rods for heating and a fan for circulating air. The temperature of the chamber was controlled through the use of an Omega temperature controller. This microprocessor-based controller could be programmed to any user-defined thermal profile consisting of a series of linear segments. A single J-type thermocouple provided feedback to the controller.

A clean aluminum pan, spatula and pincers were used for each experiment. A custom rack was used for supporting the powdered specimen placed in an aluminum pan. These were cleaned with water and then with methanol and dried for 15 minutes in a clean-air hood. A new pan was used for each experiment. An AE 100 Mettler balance with a least count of 0.1 mg was used for

weighing the sample-pan. The clean pan was weighed first, and then a sample of about 600 mg of the prepared powder was placed in it. The weighing balance was recalibrated and its leveling checked, before each experiment. The sample was then heated to 125°C and held for two hours. The pan was removed from the chamber and weighed at the end of these two hours. The sample mass obtained from this measurement was utilized as the starting sample mass during all further calculations. The chamber was then heated to the test temperature and then held there for a duration in excess of 200 hours. The test cycle temperature ramp is shown in Figure 2, where RT stands for room temperature.

The sample pan was removed periodically from the thermocycling oven for weight measurements. The pan was then weighed using the sensitive balance and then put back into the thermocycling chamber. This procedure lasted less than a minute. The test chamber temperature dropped because the door was opened twice during each measurement. However, the test temperature was restored in less than five minutes due to the large thermal mass of the chamber. As tests were conducted for more than 200 hours, and readings taken with an average gap of six hours (360 minutes) this temperature drop was not considered in further calculations and the sample was assumed to be at a steady temperature throughout the duration of the test.

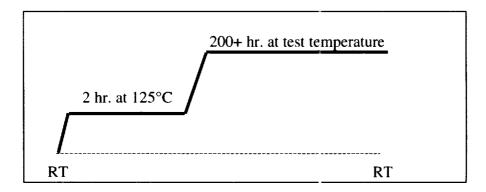


Figure 2. Long term isothermal heating cycle

A test was conducted in which a pan with powdered resin sample was held at 125°C for over 200 hours. No reactions are known to occur at this temperature and this experiment was conducted to study the extent of possible scatter and any other sources of error. The weighing balance takes a few seconds to give a steady reading. This reading can be affected by any potential moisture absorption during this period. The readings showed a variation of +1.0 mg to -1.1 mg. Lack of any trend in this data showed that the sample was not being blown away by the circulation fan and that error due to sources such as moisture absorption was small (0.2%).

ANALYSIS

A basic Arrhenius chemical reaction model is used to describe the oxidative reactions. Mass loss (or gain) is used as a degradation metric. Three different Arrhenius reactions were considered. Two of these reactions lead to mass loss whereas one reaction leads to mass gain. The analysis is implemented through the use of an explicit time-step finite difference computer code. Degradation state of the material is calculated as a function of exposure time and temperature. The analysis was used to reduce mass loss data from powdered specimens to a set of chemical reaction constants.

In the notation of Cunningham [1], the reaction is considered to take place inside an infinitesimal control volume containing a mass m_a of matrix material. The fibers are assumed to be stable. The matrix material is assumed to consist of different components that are available for various reactions. A mass m_i is defined as the mass that would be lost (or gained) due to the completion of a set of reactions involving component i. A mass fraction y_i is defined as the ratio between the mass of component i and the overall mass

$$y_i = \frac{m_i}{m_i} \tag{1}$$

A conversion metric α_i is used to keep track of the degradation of mass fraction y_i . When α_i is equal to zero, no degradation has taken place; when α_i is equal to one, the mass fraction is entirely lost (or gained). The rate at which mass is lost (or gained) from the control volume due to degradation of component i is

$$\frac{\partial m_i}{\partial t} = -m_o y_i \frac{\partial \alpha_i}{\partial t} \tag{2}$$

The total mass lost from component i is

$$\Delta m_i = \int_0^t \frac{\partial m_i}{\partial t} \tag{3}$$

Finally, the mass lost from the control volume is

$$\Delta m = \sum_{all} \Delta m_i \tag{4}$$

Arrhenius reaction kinetics are assumed for the chemical reactions acting on the different mass fractions. Reaction rates for each material component i are related to the conversion metric, α_i , and to the absolute temperature, T, by different and independent functions. A complete kinetic description of a chemical reaction requires the characterization of both [6] the rate (temperature-dependence) function, and the conversion-dependence function. The rate functions is described as

$$F(T) = k_i \exp\left(\frac{-E_i}{RT}\right) \tag{5}$$

where k_i is the reaction rate constant, E_i is the activation energy that represents the energy barrier which must be surmounted during transformation of reactants into products, and R is the real gas constant. The conversion-dependence function is expressed as $(1-\alpha_i)^{n_i}$ assuming n_i th-order kinetics, where n_i is the order of the reaction. The total reaction rate is then described by

$$\frac{\partial \alpha_i}{\partial t} = k_i (1 - \alpha_i)^{n_i} \exp\left(\frac{-E_i}{RT}\right)$$
 (6)

This is the basic form of the equation used in the model. Further details of the modeling are found in reference [1].

FIT PROCEDURE

A three reaction model was used to correlate the analytical model with the experimental data. All three reactions were assumed to be oxidative, as all the test were conducted in air. Observations indicated two mass loss and one mass gain reaction would be required to model the data. Some of these reactions appeared to reach saturation (no further mass loss/gain observed). The mass fractions y_i for the reactions which show saturation behavior were estimated from observed data. One of the reactions did not show saturation. The mass fraction on which this reaction acts was estimated on the basis of curve-fitting and observations recorded in [1]. The reaction coefficients for this model (k_i, n_i) and E_i) were obtained by using a least squares fit to different data sets. A standard optimization tool available in MATLAB (version 5.2) was used for this purpose. This tool makes use of the Levenberg-Marquardt method.

EXPERIMENTAL RESULTS

The experimental results for long term isothermal tests in air are shown in Figures 3 and 4. The normalized mass loss is plotted against the time in hours. The original mass was obtained from the weighing of the sample after heating it for 2 hours at 125°C. The mass loss observed was normalized with respect to original sample mass for each experiment. No mass loss or gain trend is observed at 125°C.

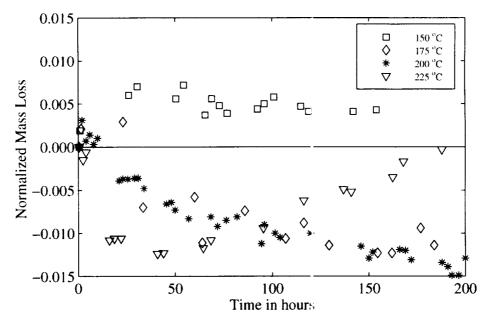


Figure 3. Long term isothermal test data for temperatures from 125-225°C

Mass loss is observed at 150°C. Mass gain is observed at 175°C and 200°C. The total mass gain seems to saturate beyond a duration of 200 hours. At 225°C, a transition from mass gain to mass loss can be seen. The mass loss behavior dominates for all higher temperatures, as shown in Figure 4.

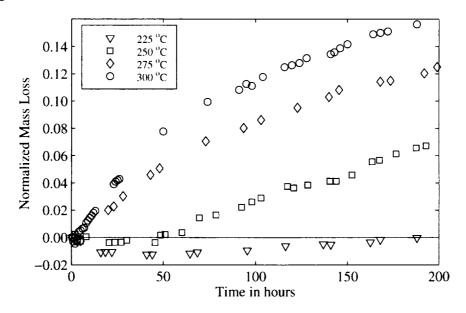


Figure 4. Long term isothermal test data for temperatures from 225-300°C

CORRELATION

The coefficients for the three reactions in the model and the mass fractions on which they act were obtained from the experimental observations. We assumed a small mass loss reaction (see 150°C), a small mass gain reaction (see 175-200°C), and a mass loss reaction that affected a large mass fraction. The saturation behavior seen in 150-200°C test was utilized for obtaining the mass fractions for the two small mass change reactions. The large mass fraction for the third reaction was estimated using a numerical search.

The three coefficients for each reaction consisting of rate constant K_i , reaction order n_i , and activation energy E_i were estimated using a optimization procedure in two steps. In the intermediate step, each reaction was modeled using C_i and n_i , where

$$C_i = k_i \exp\left(\frac{-E_i}{RT}\right) \tag{7}$$

A least squares fit was obtained for each data set. The reaction order n_i values obtained from each data set for three different reactions were found to be in a narrow range. In the next step, each reaction was quantified using all the three coefficients and with constraints placed on the reaction order variables. The least squares error from each data set was normalized by the mean mass loss (or gain) value observed. The sum of these error values was minimized using a constrained optimization approach. The coefficients obtained are listed in Table 1. The curves generated using these reaction coefficients are plotted along with the data in Figures 5, 6 and 7.

Table I - Results of Optimization for Three Reaction Model

	1	2	3	
Mass fraction v_i	0.008	-0.026	0.35	
Rate constant k_i	12.8×10^8	8.67×10^8	9.65×10^8	
Activation energy E_i (KJ/mol)	109	124	155	
Reaction order n.	1.0	2.1	3.6	

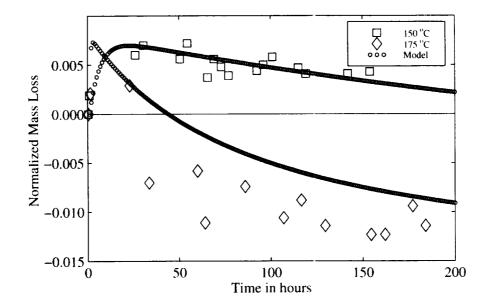


Figure. 5 Comparison of model and data for 150-175°C

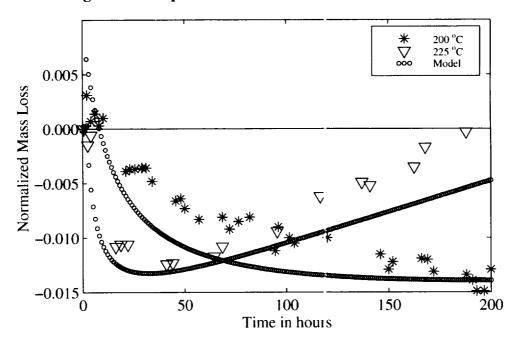


Figure. 6 Comparison of model and data for 200-225°C

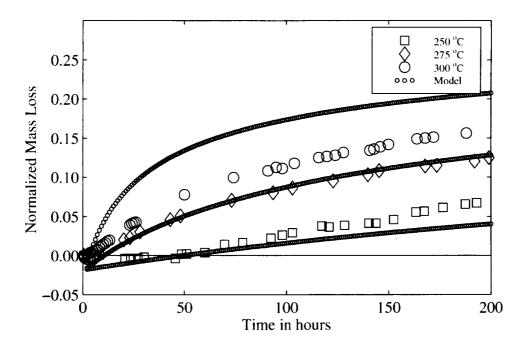


Figure. 7 Comparison of model and data for 250-300°C

CONCLUSIONS

The newly developed test method is a useful way of precisely measuring the mass loss/gain behavior and is cost-effective for long duration isothermal tests. The three reaction model is able to capture the mass loss and gain trends reasonably well. The mass gain behavior, not captured in previous models, is adequately quantified in this new model. The model does not succeed in capturing the behavior at 300°C. This is thought to be because of a transition from low temperature to high temperature behavior. Higher temperature behavior is captured by the model of Cunningham [1]. The new model used in conjunction with the previous model, captures material degradation behavior at all temperatures of interest.

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